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Irving M. Fishman

Type or Print Name

## IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

IN RE APPLICATION OF

Confirmation No. 8854

Nagi Awad

Group Art Unit: 1712

SERIAL NO: 10/646,122

Examiner: Marc S. Zimmer

FILED: Aug 22, 2003

FOR: CROSS-LINKED SILICONE GELS, PRODUCTS

CONTAINING THE SAME, AND METHODS OF

MANUFACTURE THEREOF

**Assistant Commissioner for Patents** 

Alexandria, VA 22313-1450

# Submission of Corrected Re-executed Awad Declaration

Sir:

Further to Applicant's amendment dated January 18, 2005 Applicant submits a newly executed corrected Awad Declaration. The Declaration previously submitted with the amendment of January 18, 2005 contained hand corrections made by Dr. Awad, but dated after the date of execution. As such, the undersigned prepared a new copy of the Declaration with the corrections made and has had Dr. Awad re-execute the revised Declaration.

Applicant submits that the Application is now in allowable form and respectfully requests that it be passed to issue.

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Dated: January 19, 2005

Respectfully submitted,

Irving M. Fishman

Reg. No. 30258

Attorney Docket: 119.002

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IN RE APPLICATION OF

Nagi M. Awad : Examiner: Marc S Zimmer

SERIAL NO.: 10/646,122 : Art Unit: 1712

FILED: August 22, 2003

FOR: CROSS-LINKED SILICONE GELS;

PRODUCTS CONTAINING THE SAME;

AND METHODS OF MANUFACTURE

THEREOF :

Assistant Commissioner for Patents
United States Patent and Trademark Office
PO Box 1450
Alexandria, VA 22313-1450

## DECLARATION of Nagi M. Awad

## Dear Sir:

I, Nagi M. Awad, residing at 322 Freeman's Lane, Franklin Lakes, NJ 07417, hereby declare and say as follows:

- I graduated from Ain Shams University, Cairo, Egypt in 1962, having obtained a
  Bachelor of Science degree in Chemistry.
- 2. From then until 1968, I was an Industrial Research Fellow in the Chemistry Department of the Ministry of Industry, Cairo, Egypt.

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3. In 1968, I also graduated from Cairo University, Cairo, Eqypt, having obtained a Bachelor of Science degree in chemical Engineering.

- 4. In 1969, I graduated from Ain Shms University, Cairo, Egypt, having obtained a Master of Science degree in Physical Chemistry
- 5. From then until 1976, I was employed as R&D manager of Nice Pak, Mount Vernon, NY where among other things, my duties includeddeveloping a line of alcohol-free wet towelette products.
- 6. From then until 1984, I was employed as a Research Director at Hydrolabs,
  Patterson, NJ, where my duties involved, among other things, development of a
  line of textile auxiliaries..
- 7. In 1980, I also graduated from Polytechnic Institute of Brooklyn, Brooklyn, NY, having obtained a PhD degree in Polymer Chemistry.
- 8. From 1984 to the present I have been the founder and President of NuTech Corporation, Newark, NJ, a mid-sized specialty chemical business that focuses on development of novel products to improve industrial processes. Representative products have included defoamers used in textile dyeing, inks, paint preparation, cutting oils, formulations for shaping metal components, cosmetic silicone gels.
- 9. I am the inventor of US Ser. No. 10/646,122, filed August 22, 2003, the current pending application
- 10. I have read and am familiar with the outstanding Office Action of November 24, 2004.

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11. I give this declaration to demonstrate to the Examiner that the process steps of continued mixing with a large blade throughout polymerization leads to a different product with different properties than mixing is halted when gelling is visually noticed or when mixing is accomplished with a small blade. The present Declaration is also provided to present to the Examiner additional details about the monomers used in the polymerizations.

- In all of the following reported experiments as well as in all of the formulations discussed in the previously presented IDSs in the present application, the α,ω-divinylpolydimethylsiloxane used was the same material having a molecular weight of 22,500±2,250, the polymethylhydrosiloxane varied between materials having molecular weights nominally mentioned as (a) 3,756, (b) 3,756, and (c) 3,785. The undersigned is not aware of the range of the molecular weight present in each of these materials; and the α,ω-divinylpolydiphenyldimethylsiloxane was of average molecular weight of about 18,900, but the manufacturer did not designate the range of molecular weights in the product.
- 13. The following components were used in all of the comparison formulations presented in this declaration:

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#### TABLE I

Component	% of formulation for polymerization
1) Pentameric Cyclomethicone	94.005
2) α,ω-divinylpolydimethylsilox	ane 5.19
3) Polymethylhydrosiloxane	0.411
4) Platinum catalyst in	0.00393
<u>α,ω-divinylpolydimethylsilox</u>	ane 0.389
Total polymerization mixture	99.99893

- 14. Sample A is prepared by blending the above components 1-4 in a Kitchen Aide Dough Mixer on a fast mixing setting using a large blade. Sample A is allowed to continue mixing until polymerization is complete. This represents the Kuwata practice.
- 15. Sample B is prepared by blending the above components 1-4 in a Kitchen Aide Dough Mixer on a fast mixing setting using a large blade; however, when gelling is first visually noticed, the mixing is halted and the mixture is allowed to complete polymerization without further mixing. This represents the process used in the claim 1 of the present invention except that cyclomethicone is the polymerization medium instead of the invention hydrocarbon.
- 16. Sample C is prepared by blending the above components 1-4 in a Kitchen Aide Dough Mixer on a fast mixing setting using a small blade. Sample C is allowed to continue mixing until polymerization is complete; however, because only a small blade is used, only a relatively small portion of the mixture is moved as the blade turns through the mass. This embodiment represnts the process used in the instant invention claim 34 except that cyclometicone is used as the polymerization medium instead of the invention hydrocarbon.

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- 17. Once polymerization is complete, each of these Samples A-C respectively is passed through a colloid mill to obtain a paste (Pastes A-C, respectively). The settings on the colloid mill are identical for each sample.
- 18. Each Paste is then blended as set forth in Table II:

#### TABLE II

Product & Lot	Product A	Product B	Product C
Paste	58.93% Paste A	58.93% Paste B	58.93% Paste C
Hydrogenated polyisobutene	230.89%	30.89%	30.89%
Pentameric cyclomethicone	10.08%	10.08%	10.08%
Total Product	99.9	99.9	99.9

19. The clarity, viscosity of the Product, and viscosity of the Product further diluted with 5% hydrogenated polyisobutene is set forth below.

## TABLE III

		Product	viscosity on dilution with
Product	<u>Appearance</u>	viscosity	5% hydrogenated polyisobutene
Α	hazy	36,000 cps	10,000 cps
В	clear	220,000 cps	136,000 cps
C	clear	232,000 cps	140,000 cps

20. As can be readily seen, the product obtained from the presently claimed invention processes (except that cyclomethicone is used instead of the invention hydrocarbon as the polymerization medium) has different properties than that obtained by the process used in making Product A, notwithstanding that each of

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the Products have the same Formulation Components in the same amounts. Thus, the mere difference of adhering to the invention shear control properties during polymerization as opposed to not doing so results in very different products, products with properties that would not have been obvious based on the prior art.

The undersigned declares further that all statements made herein of his own knowledge are true and that all statements made on information and belief are believed to be true and further that these statements are made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the Unite States Code and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

Signed at Newark, NJ, this 18th day of January, 2005.

Nagi M. Awad